Derivation of compressible two-phase flow models with surface tension

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Motivations



Context

- Nuclear safety: accident situation in pressurized water reactor
- High temperature and pressure conditions
- Compressible two-phase flows (or multiphase flows) with heterogeneities (bubbles, droplets...)
 - Complex interface
- Thermodynamical (dis)equilibrium
 - Thermal, mechanical, mass transfers through the interface
- Complex wave interactions (shocks, phase transition...)

The richest model [Baer, Nunziato '86]

- Euler system for two immiscible phases k = 1, 2 with coupling terms
- Phasic state $w_k = (\rho_k, u_k, e_k)$, $w = (w_1, w_2)$
- Pressure $p_k = p_k(\rho_k, e_k)$, total energy $E_k = e_k + \frac{u_k^2}{2}$, chemical potential $\mu_k = \mu_k(\rho_k, e_k)$
- Volume fraction $\alpha_k \in [0, 1]$

$$\begin{aligned} \alpha_1 + \alpha_2 &= 1 \qquad \rho = \alpha_1 \rho_1 + \alpha_2 \rho_2 \\ \partial_t \alpha_1 + u_i(w) \partial_x \alpha_1 &= \lambda_p(w)(p_1 - p_2) \\ \partial_t(\alpha_k \rho_k) + \partial_x(\alpha_k \rho_k u) &= \lambda_\rho(w)(\mu_l - \mu_k) \\ \partial_t(\alpha_k \rho_k u_k) + \partial_x(\alpha_k \rho_k u_k^2 + \alpha_k p_k) - p_i(w) \partial_x \alpha_k &= \lambda_u(w)(u_l - u_k) \\ \partial_t(\alpha_k \rho_k E_k) + \partial_x((\rho_k E_k + p_k) \alpha_k u) + p_i(w) \partial_t \alpha_k &= \lambda_u(w) u_i(w)(u_l - u_k) \end{aligned}$$

- ✓ Well-posedness although nonconservative: hyperbolicity, symmetrizable, jump conditions...
- X Heuristic closure laws for interfacial quantities $u_i(w)$ and $p_i(w)$
- ★ Empirical relaxation time scales $\lambda_{p,\rho,u}(w)$ and source terms, possibly depending on interfacial area...

Motivations



Derivation of consistent models

- Macroscopic description
 - Derive average models
- Conserve informations from the interface scale
 - Interfacial area, surface tension...
- Mathematical structure
 - Well-posedness (smooth solutions, discontinuities...)

Comparison of two possible derivations

One-velocity framework



[Serre '91 & '01, E '92, Hillairet '07, Bresch & Huang '11, Bresch & Hillairet '15 & '19, Hillairet '18, Bresch, Burtea & Lagoutière '20]

From micro to macro...

- Microscopic description of the mixture
 - Viscous flows (smooth enough solutions) for both phases
 - Conditions through the interfaces ("perfect transducers")
- One-fluid model with high-oscillatory density solutions
- \blacktriangleright Pass to the limit to deduce macroscopic quantities $\alpha_{1,2},\rho_{1,2},\rho$ and u

Pros & Cons

- ✓ Fully rigorous
- X Restrictive interface conditions

[Serre '91 & '01, E '92, Hillairet '07, Bresch & Huang '11, Bresch & Hillairet '15 & '19, Hillairet '18, Bresch, Burtea & Lagoutière '20]

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Goal [Hillairet, M. & Seguin '23]

- \checkmark Introduce more complex interface behavior \rightsquigarrow surface tension
- ✓ Couple different fluid models

The one-dimensional microscopic model

Assumptions for the microscopic model (first in 3D)

- Fluid f, N bubbles of gas g, $n \in \{1, \ldots, N\}$
- Compressible Navier-Stokes equations for both phases
- Bubbles remain spherical (translation, dilatation, rotation)
- Interface conditions
 - Continuity of the velocity field
 - Surface tension

$$\begin{aligned} u_f &= u_n \\ (\Sigma_f - \Sigma_n) \nu &= \kappa_n \nu \end{aligned}$$

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$$\begin{aligned} u_f &= u_n\\ (\Sigma_f - \Sigma_n) &= \gamma/R_n \end{aligned}$$

In 1D



▶ In the fluid domain $\mathcal{F}(t)$

 $\blacktriangleright \ \rho_f, \, u_f, \, \Sigma_f = \lambda_f \partial_x u_f - \mathbf{p}_f(\rho_f)$

- ▶ In each buble $B_n(t) = B(c_n(t), R_n(t))$
 - Constant mass m_n and Newton laws

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- Well posedness of the Cauchy problem for a time T > 0, depending on N...

Microscopic initial data

Provide the initial gas-bubble distribution

 \blacktriangleright Probability distribution of the bubbles, in position x and radius r

 $S_g^0 = S_g^0(x, r) \in L^1(\Omega \times \mathbb{R}^+)$

First moments of S_g^0

• 1-st order moment \rightsquigarrow volume fraction

$$\boldsymbol{\alpha_g^0}(x) = \int_{\mathbb{R}^+} (2r) S_g^0(x, r) \mathrm{d}r$$

▶ 0-th order moment (~> gas covolume, "interfacial area")

$$\boldsymbol{a}^{0}(x) = \int_{\mathbb{R}^{+}} S_{g}^{0}(x, r) \mathrm{d}r$$

Family of microscopic initial data to be constructed from S_g^0 , ρ_f^0 and u_f^0

- ► For any bubble number N ≥ 1:
 - 1. From S_g^0 deduce $(c_n^{(N),0}, R_n^{(N),0})_{n=1,\dots,N}$
 - 2. Use velocity continuity to define $\dot{c}_n^{(N),0}$, $\dot{R}_n^{(N),0}$

Solve the microscopic model

Scaling

• m_n , R_n^0 , $|\mathcal{F}_n^0|$ and γ behave as N^{-1}

Microscopic Cauchy problem independent of N [Hillairet, M., Seguin '23]

Consider compatible initial data and the above scaling. Then there exists $T_\infty>0,$ independent of N, such that

$$\left(\rho_{f}^{(N)}, u_{f}^{(N)}, (c_{n}^{(N)}, R_{n}^{(N)})_{n=1,\dots,N}\right)$$

exists and is unique

- T_{∞} taken smaller and smaller along the proof
- \blacktriangleright Combine energy and regularity estimates, independent of N
- \blacktriangleright Smoothness of the velocity $u_{f}^{(N)}$ obtained by extended stress tensors

Fluid unknowns

- Characteristic function of the fluid domain $\chi^{(N)}=\mathbf{1}_{\mathcal{F}^{(N)}}$, density $\rho_1^{(N)}=\rho_f^{(N)}$

Gas unknowns

• Density
$$\rho_2^{(N)} = \sum_{n=1}^N \rho_n^{(N)} \mathbf{1}_{B_n}$$
 with $\rho_n^{(N)} = m_n^{(N)} / (2R_n^{(N)})$

• Interfacial area/covolume $a^{(N)} = \sum_{n=1}^{N} a_n^{(N)} \mathbf{1}_{B_n}$ with $a_n^{(N)} = 1/(2NR_n)$

Mixture unknowns

• Density
$$\rho^{(N)}$$
 and velocity $u^{(N)}$

Fluid unknowns

- Characteristic function of the fluid domain $\chi^{(N)}=\mathbf{1}_{\mathcal{F}^{(N)}}$, density $\rho_1^{(N)}=\rho_f^{(N)}$

Gas unknowns

- Density $\rho_2^{(N)} = \sum_{n=1}^N \rho_n^{(N)} \mathbf{1}_{B_n}$ with $\rho_n^{(N)} = m_n^{(N)}/(2R_n^{(N)})$
- Interfacial area/covolume $a^{(N)} = \sum_{n=1}^{N} a_n^{(N)} \mathbf{1}_{B_n}$ with $a_n^{(N)} = 1/(2NR_n)$

Mixture unknowns

 \blacktriangleright Density $\rho^{(N)}$ and velocity $u^{(N)}$

Methodology

- Using relative compactness (up to extraction of subsequences)
- ▶ Pass to the limit in nonlinear combinations of $\chi^{(N)}(t,x)$, $\rho^{(N)}(t,x)$ and $a^{(N)}(t,x)$
- \checkmark Nonlinear convergence in the sense of Young measures
- \rightsquigarrow Evolution equations on fluid, bubble and mixture unknowns

The macroscopic model

Macroscopic closed system

$$\begin{cases} \alpha_1 + \alpha_2 = 1, & \rho = \alpha_1 \rho_1 + \alpha_2 \rho_2 \\ \partial_t \alpha_1 + u \partial_x \alpha_1 = \frac{\alpha_2 \alpha_1}{\alpha_1 \lambda_2 + \alpha_2 \lambda_1} \left[(\lambda_2 - \lambda_1) \partial_x u + (\mathbf{p}_1(\rho_1) - \mathbf{p}_2(\rho_2)) - \bar{\gamma} \frac{a}{\alpha_2} \right] \\ \partial_t a + \partial_x (au) = 0 \\ \partial_t (\alpha_1 \rho_1) + \partial_x (\alpha_1 \rho_1 u) = 0, & \partial_t (\alpha_2 \rho_2) + \partial_x (\alpha_2 \rho_2 u) = 0 \\ \partial_t (\rho u) + \partial_t (\rho^2 u) = \partial_x \Sigma \\ \text{with } \Sigma = \frac{\lambda_2 \lambda_1}{\alpha_1 \lambda_2 + \alpha_2 \lambda_1} \left[\partial_x u - \left(\frac{\alpha_1}{\lambda_f} \mathbf{p}_1(\rho_1) + \frac{\alpha_2}{\lambda_2} \mathbf{p}_2(\rho_2) \right) - \frac{\bar{\gamma}}{\lambda_2} a \right] \end{cases}$$

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Additional kinetic equation (Boltzmann-Williams)

- Distribution function in position and radius $S_t^{(N)} = \frac{1}{N} \sum_{k=1}^N \delta_{c_k(t), NR_k(t)}$
- Converges towards the probability distribution S_g satisfying

$$\partial_t S_g - \partial_x (S_g \bar{u}) + \frac{1}{\lambda_2} \partial_r ((r(\Sigma_2 + p_2(\rho_2)) + \bar{\gamma}/2) S_g) = 0$$

• 0-th order moment
$$a(t,x) = \int_{\mathbb{R}^+} S_g(t,x,r) dr$$

Comments on the macroscopic model

- ✓ Mechanical relaxation Surface tension
 a interfacial area in 3D(?)
 Additional kinetic equation
- X 3D extension

Viscous flows

1 velocity/temperature

Derivation by

Homogenization

Two possible derivations

 ✓ Mechanical relaxation Surface tension
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Derivation by Homogenization Derivation by Stationnary Action Principle [Bedford '85, Gavrilyuk & Gouin '99, Gavrilyuk & Saurel '02, Berdichevsky '09, Belozerov, Peshkov & Romenski '15...]

- Set up the assumptions that govern the physical phenomenon i.e. define kinetic and potential energies
- \blacktriangleright Lagrangian L whose integral over space-time gives the Hamiltonian Action of the system
- Evolution of the system along possible trajectories
- SAP postulate: the physical trajectory optimizes the action
- Hamiltonian and entropy structure
- X Reversible processes

Main ingredient

L = kinetic energy - potential energy

State of art

[Gavrilyuk & Saurel '02, Drui '17, Essadki '18, Cordesse '20, Di Battista '21, Kokh '21...]

- Add terms in the kinetic energy, keep geometrical informations related to small scale interface features
- X Consider surface tension as a kinetic feature
- × No particular derivation of the potential energy
- × Isothermal case

Aim

- \checkmark Consider surface tension as a thermodynamic feature
- \checkmark Provide a rigorous derivation of the potential energy

Fluid and gas phases

 Porous media literature [Smai '20, Kondepudi & Prigogine '98, Laudau & Lifshitz '78...]

Extensive description

- ▶ k = 1, 2
- Volume $V_k \ge 0$, entropy $S_k \ge 0$, mass $M_k \ge 0$
- ▶ Internal energy $E_k \in C^2((\mathbb{R}_+)^3)$
 - Convex and positively homogeneous: $\forall \lambda \in \mathbb{R}^*_+$

$$E_k(\lambda M_k, \lambda V_k, \lambda S_k) = \lambda E_k(M_k, V_k, S_k)$$

Gibbs form

$$\mathrm{d}E_k = T_k \mathrm{d}S_k - p_k \mathrm{d}V_k + \mu_k \mathrm{d}M_k$$

Pressure p_k , temperature $T_k > 0$, chemical potential μ_k

Intensive form : intensive variables relatively to the mass of the phase k

- Specific volume $\tau_k = V_k/M_k = (1/\rho_k)$ and entropy $s_k = S_k/M_k$
- Specific internal energy $e_k(\tau_k, s_k) = 1/M_k E_k(M_k, V_k, S_k)$

$$\mathrm{d}e_k = T_k \mathrm{d}s_k - p_k \mathrm{d}\tau_k$$

The interface

Assumptions

Sharp, no volume, no mass

Extensive description

- Entropy $S_i \ge 0$, area $A \ge 0$
- ▶ Internal energy $E_i(S_i, A)$ convex and positively homogeneous
- Gibbs form

 $\mathrm{d}E_i = T_i \mathrm{d}S_i + \gamma \mathrm{d}A$

- Surface tension γ
- Interfacial temperature T_i

Intensive description

- Intensive variables relatively to the volume V of the mixture
 - Interfacial area density a = A/V
- \blacktriangleright Intensive variables relatively to the interfacial area A
 - ▶ Interfacial intensive entropy $s_i = S_i/A$
 - Interfacial intensive energy $e_i = E_i/A$

The fluid-interface system

For a given state (M, V, E, A) of the system

Modeling constraints

Fluid phases are immiscible, no vacuum, interface has no volume

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1 = \alpha_1 + \alpha_2 with \alpha_k = V_k / V \in [0, 1]
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Mass conservation, interface has no mass

 $1 = y_1 + y_2$ with $y_k = M_k/M \in [0, 1]$

Entropy conservation (homogeneity)

 $1 = z_1 + z_2 + z_i$ with $z_k = S_k/S \in [0, 1], k = 1, 2, i$

System extensive internal energy

 $E(M, V, S, A) = E_1(M_1, V_1, S_1) + E_2(M_2, V_2, S_2) + E_i(S_i, A)$

Mixture potentials and equilibrium

Extended Gibbs form for the system

$$dE = (z_1T_1 + z_2T_2 + z_iT_i)dS - (\alpha_1p_1 + \alpha_2p_2 - a\gamma)dV + (y_1\mu_1 + y_2\mu_2)dM + S((T_1 - T_i)dz_1 + (T_2 - T_i)dz_2) - V((p_1 - p_2)d\alpha_1 - \gamma da) + M(\mu_1 - \mu_2)dy_1$$

Consequences

Definitions of the mixture potentials

$$egin{cases} T := z_1 T_1 + z_2 T_2 + z_i T_i \ p := lpha_1 p_1 + lpha_2 p_2 - a \gamma \ \mu := y_1 \mu_1 + y_2 \mu_2 \end{cases}$$

• At thermodynamical equilibrium, for a given state (M, V, E, A), the mixture energy E reaches a minimum

$$\begin{cases} \mu_1 = \mu_2 \\ T_1 = T_2 = T_i \\ \gamma da - (p_1 - p_2) d\alpha_1 = 0 \end{cases}$$

Potential energy candidate

Potential energy accounting for interfacial informations [M. '24]

$$e(\tau, s, s_1, s_2, a, \alpha_1, y_1) = y_1 e_1 \left(\frac{\alpha_1}{y_1}\tau, s_1\right) + (1 - y_1) e_2 \left(\frac{1 - \alpha_1}{1 - y_1}\tau, s_2\right) \\ + a\tau e_i \left(\frac{s - y_1 s_1 - (1 - y_1) s_2}{a\tau}\right)$$

where

s is the system specific entropy

 $s = y_1 s_1 + (1 - y_1) s_2 + a\tau s_i$

Kinetic energy

kinetic energy
$$=rac{1}{2}
ho |\mathbf{u}|^2 + oldsymbol{ heta}$$

Kinetic energy of translational motion +small scale kinetic energy

[Gavrilyuk & Saurel '02, Drui '17, Cordesse '18, Di Battista '21, Loison '23...]

 $\theta = m(a) |D_t \alpha_1|^2$ with $D_t \cdot = \partial_t \cdot + \mathbf{u} \cdot \nabla \cdot$

Here consider

$$\theta = \frac{1}{2}m|D_t\alpha_1|^2 + \frac{1}{2}\nu|D_ta|^2$$

Physical interpretation

Pulsation energy results in both volume and interfacial area variations

(A posteriori) Mathematical argument

• Mandatory to get evolution/transport equations on α_1 and a

Kinetic energy

kinetic energy
$$= \frac{1}{2} \rho |\mathbf{u}|^2 + \boldsymbol{\theta}$$

Kinetic energy of translational motion +small scale kinetic energy

Gavrilyuk & Saurel '02, Drui '17, Cordesse '18, Di Battista '21, Loison '23...]

 $\theta = m(a) |D_t \alpha_1|^2$ with $D_t \cdot = \partial_t \cdot + \mathbf{u} \cdot \nabla \cdot$

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Mandatory to get evolution/transport equations on α₁ and a

Moral

Kinetic energy encodes the final set of PDEs

 Potential energy encodes the pressure and source terms (via the extended Gibbs form)

Lagrangian, assumptions and SAP

Lagrangian

$$L(\mathbf{B}) = \frac{1}{2}\rho|\mathbf{u}|^2 + \frac{1}{2}m|\mathbf{D}_t\alpha_1|^2 + \frac{1}{2}\nu|\mathbf{D}_ta|^2 - \rho e(\tilde{\mathbf{B}})$$

Some additional assumptions/constraints

- Mass conservations
 - Density of the system $\rho = 1/\tau$: $\partial_t \rho + \operatorname{div}(\rho \mathbf{u}) = 0$
 - Mass fraction y_1 : $D_t y_1 = 0$

Specific entropy conservation along trajectories

$$D_t s = 0 \quad \text{and} \quad D_t s_k = 0, \qquad k = 1, 2$$

 \rightsquigarrow Interface entropy s_i is not advected

Choice of variables to depict the system

 $(x,t) \mapsto \mathbf{B} = (\rho, s, s_1, s_2, a, \alpha_1, y_1, \mathbf{u}, \mathbf{D}_t \alpha_1, \mathbf{D}_t a)$

Stationary Action Principle

- Integral of L defines the Hamiltonian Action of the system
- Family of transformations such that the constraints hold
- Physically relevant transformation optimizes the Action

Conservative PDE system

Evolution equations [Di Battista '21, M. '24]

SAP leads to

$$\begin{cases} \partial_t M + \operatorname{div}(M\mathbf{u}) - \frac{\partial L}{\partial \alpha_1} = 0 & \text{with } M = \frac{\partial L}{\partial (D_t \alpha_1)} \\ \partial_t P + \operatorname{div}(P\mathbf{u}) - \frac{\partial L}{\partial a} = 0 & \text{with } P = \frac{\partial L}{\partial (D_t a)} \\ \partial_t K + \operatorname{div}(K\mathbf{u}) - \nabla L^{*,\rho} = 0 & \text{with } K = \frac{\partial L}{\partial \mathbf{u}} \text{ and } L^{*,\rho} = \rho \frac{\partial L}{\partial \rho} - L. \end{cases}$$

Moreover if

 $E(\rho, K, M, P, s, s_1, s_2, y_1) =$ kinetic energy + potential energy

is convex, then the system is hyperbolic and symetrizable.

- Godunov-Mock argument
- X Sufficient criterion quite restrictive

Extended equations

► By definition of *L*(**B**)

▶ Equation on $K = \partial L / \partial \mathbf{u} = \rho \mathbf{u}$ gives the momentum equation

$$\partial_t(\rho \mathbf{u}) + \mathsf{div}(\rho \mathbf{u}^\top \mathbf{u}) + \nabla \left(p + \frac{m}{2} |D_t \alpha_1|^2 + \frac{\nu}{2} |D_t a|^2 \right) = 0$$

with

$$p = \alpha_1 p_1 + (1 - \alpha_1) p_2 - a\gamma$$

• Two second order conservative equations on $M = mD_t\alpha_1$ and $P = \nu D_t a$

$$\begin{cases} D_t \alpha_1 = \partial_t \alpha_1 + \mathbf{u} \cdot \nabla \alpha_1 = \frac{\rho y_1 w}{\sqrt{m}} \\ \partial_t w + \mathbf{u} \cdot \nabla w = \frac{1}{\sqrt{m} \rho y_1} (p_2 - p_1) \\ D_t a = \partial_t a + \mathbf{u} \cdot \nabla a = \frac{\rho y_1 n}{\sqrt{\nu}} \\ \partial_t n + \mathbf{u} \cdot \nabla n = \frac{\gamma}{\sqrt{\nu} \rho y_1} \end{cases}$$

Equations on w and n refer to small scale momentum equation
 Equations on a₁ and a connect small and large scales

Comparison to similar models

Final set of equations [M. '24]

$$\begin{cases} \alpha_{1} + \alpha_{2} = 1, \quad \rho = \alpha_{1}\rho_{1} + \alpha_{2}\rho_{2}, \quad p = \alpha_{1}p_{1} + (1 - \alpha_{1})p_{2} - a\gamma \\ \partial_{t}\rho + \operatorname{div}(\rho\mathbf{u}) = 0 \\ \partial_{t}(\rho\mathbf{u}) + \operatorname{div}\left(\rho\mathbf{u}^{\top}\mathbf{u} + \left(p + \frac{m}{2}(\rho y_{1}w)^{2} + \frac{\nu}{2}(\rho y_{1}n)^{2}\right)\mathbf{Id}\right) = 0 \\ \partial_{t}\alpha_{1} + \mathbf{u}^{\top}\nabla\alpha_{1} = \frac{\rho y_{1}w}{\sqrt{m}} \\ \partial_{t}a + \mathbf{u}^{\top}\nabla a = \frac{\rho y_{1}n}{\sqrt{\nu}} \\ \partial_{t}w + \mathbf{u}^{\top}\nabla w = \frac{1}{\sqrt{\frac{\nu}{\gamma}\rho y_{1}}}(p_{2} - p_{1}) \\ \partial_{t}n + \mathbf{u}^{\top}\nabla n = \frac{\gamma}{\sqrt{\nu}\rho y_{1}} \end{cases}$$

Formal asymptotics

- $\gamma, \nu \rightarrow 0$ and isothermal case: [Drui *et al '17*]
- $O(\sqrt{\nu}, \sqrt{m})$: [Kokh *et al '19*], recover almost the model of part 1

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X 3D extension

Viscous flows

1 velocity/temperature

Derivation by Homogenization Derivation by Stationnary Action Principle

✓ Mechanical relaxation
 Surface tension, interfacial area
 Two temperatures
 Possibly two velocities

X Lack of dissipative terms Provide relaxation terms to close the system

To sum up

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 a interfacial area in 3D(?)
 Additional kinetic equation
- X 3D extension

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Thank you for your attention!